The world's first Taylor Reactor



LCTR[®]-series



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Global New Technology

Pioneered in the new field of chemical reactor

Since the establishment in 2010, Laminar Co., Ltd based on Technology has developed a new concept of chemical reactor named as Taylor Reactor(LCTR, Laminar Continuous Taylor Reactor) and pioneered in the new fields of chemical reactors. Furthermore, going on to enlarge the general reactor market fields.

To satisfy the needs of all customers, we are continuously studying research and doing the development of reactors. Resultantly, Laminar possesses the best manufacturing know-hows and a number of Technologies.

The custom made Taylor reactors are also possible as per the special requirements from the chemical manufacturing processes, based on several technologies and know-hows.

reactors.

Due to innovative R&D activity, we are developing the new functional chemical reactor fields





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ISO 9001











Laminar Co., Ltd.

As already proved reactor in functionality and reliability in the market, Taylor reactor is exporting abroad from 2013, and now Laminar Co., Ltd is enlarging widely the business fields for Taylor

Laminar

Taylor fluid flow

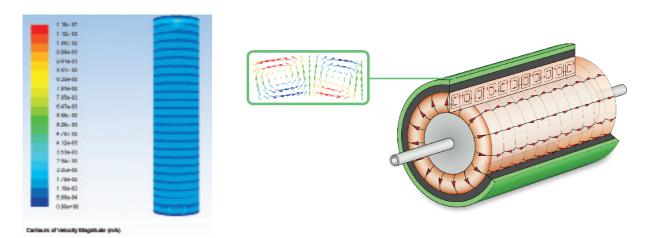
The reactor session is made up with two cylinders, inside and outside, and the solution to be reacted is fed into the space between the inside and the outside cylinder through the feeding ports.

As soon as the inside cylinder is rotated by the motor, the solution is also starting to move and then forming a strong stream in the direction of rotation.

Simultaneously, two forces of Centrifugal and Coriolis are generated so strongly that the solution in the reactor moves fast for the outside cylinder.

The faster the inside cylinder is rotated, The more unstable the flow comes to be.

By this phenomena, the eddy current flow is created regularly in the shape of the double rings each of which is self-rotated in the opposite direction, along the rotated inside cylinder. It is shaped like a band in the reactor. This means a Taylor flow in which is called.



Cathode material of Lithium ion battery, precursor

Class	Batch Reactor	LCTR [®] Reactor
Fluid mixing method	Macro-mixing	Micro-mixing
Mass transfer velocity (m/s)	1	3.3
Mixing intensity (W/kg)	0.8	5.8
Reaction time (h)	16	2
Span([D ₉₀ -D ₁₀]/D ₅₀)	0.5	0.2
Tap Density(g/mL)	2.1	2.2

A Taylor fluid flow can generate a turbulent flow easily by changing the rotational speed of an inner cylinder, so it is much used to study the stability of a fluid. Rayleigh performed a stability analysis for a non-viscous fluid for the first time

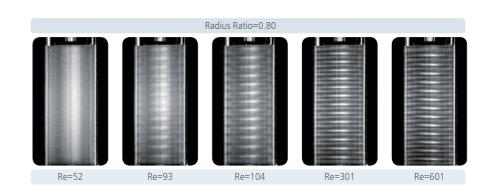
For a viscous fluid, Taylor reported that a Taylor vortex occurs in a domain larger than the critical Taylor number based on linear theory. The instability condition of a flow can be represented as a Taylor number(Ta), which is defined by a rotational direction Reynolds number and a reactor shape factor(d/r_i) as follows:

 $Ta = \frac{\omega_i r_i d}{v}$

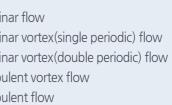
where d is the distance between two cylinders, r_i is the radius of the inner cylinder, ω_i is the rotational angular speed of the inner cylinder, and v is the dynamic viscosity of the fluid.

Taylor presented that the critical Taylor number (Ta_c) as d/r_i approaches 0 is 41.3, and Kataoka et al. classified the flow characteristics based on a Taylor number when d/r_i is 0.62 without axial flow as follows:

Ta <ta<sub>c</ta<sub>	: lamin
Ta _c <ta<800< th=""><th>: lamin</th></ta<800<>	: lamin
800 <ta<2000< th=""><th>: lamin</th></ta<2000<>	: lamin
2000 <ta<10000~15000< th=""><th>: turbu</th></ta<10000~15000<>	: turbu
Ta>15000	: turbu

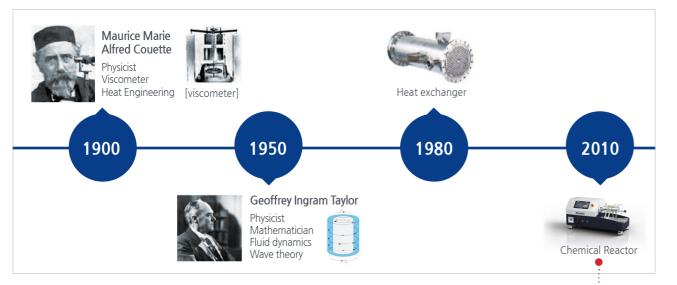


$$\left(\frac{d}{r_i}\right)^{1/2}$$

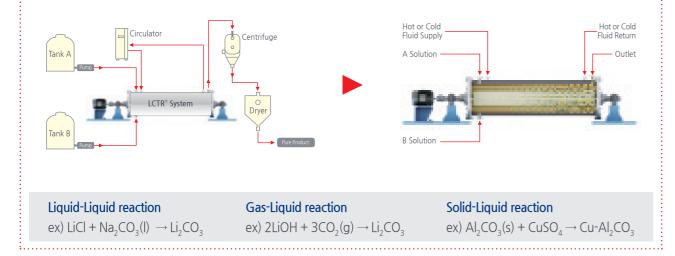


LCTR[®] system

HISTORY

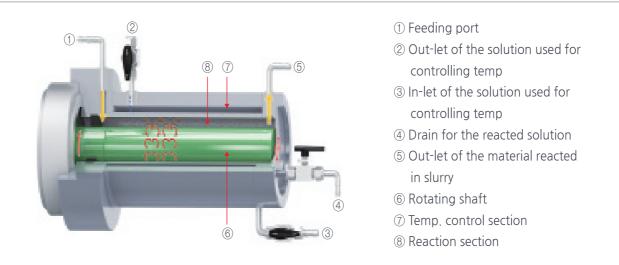


LCTR[®] is possible to manufacture the new materials by feeding Gas, Liquid and Solid under the condition of the presence of solvent.

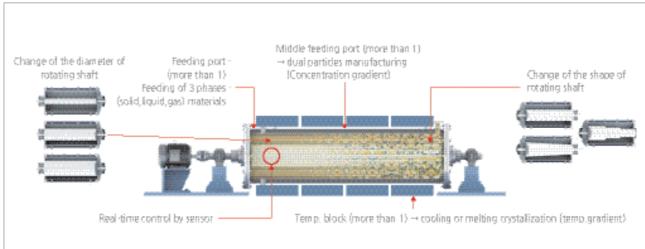


LCTR[®] Inner structure and manufacturing option

Inner structure



Manufacturing option

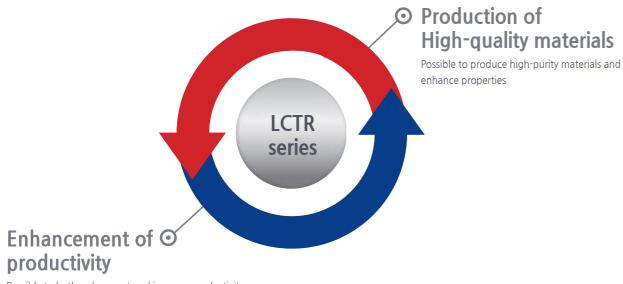


Characteristics of LCTR[®]-series

LCTR[®]: Batch + Tubular



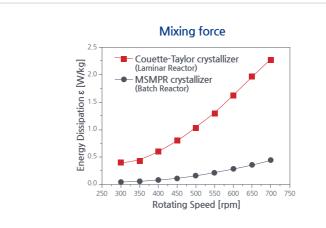
The development of a ideal chemical reactor functioning the continuous manufacturing system for high purity materials by utilizing fully the advantages of both Batch (easy to operate, the use of mixer, easy to check in operation) and Tubular (high purity production, high reproducibility, east to produce nano-materials)



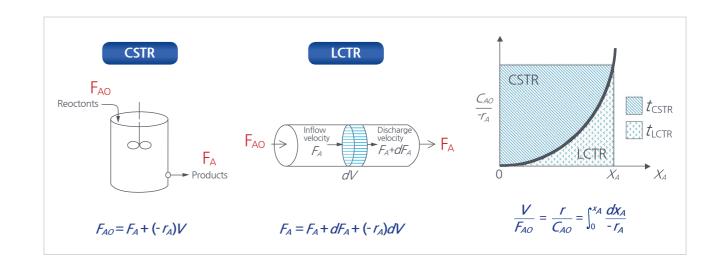
Possible to both reduce cost and increase productivity due to shortened reaction time and continuous production system.

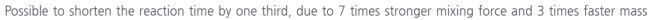
Time reduction

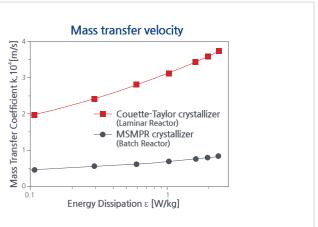
Possible to shorten the reaction time by one third, due to transfer velocity



Nguyen-Anh TUAN, Jeong-ki Kang, Jong-Min Kim, Sang-Mok CHANG, Choul-Ho Lee, Woo-sik KIM, "Drowning-out Crystallization of Guanosine 5-Monophosphate(GMP) in Continuous Couette-Taylor Crystallizer" 8th International Conference on Separation Science and Technology, Karuizawa, Japan, (Oct 2-4, 2008)



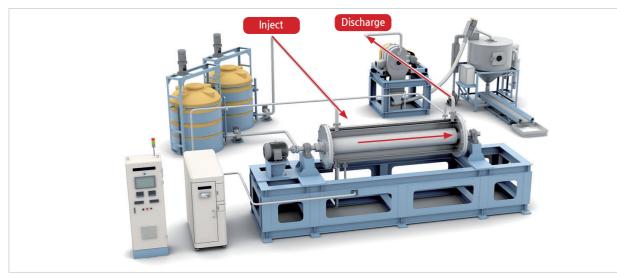




Characteristics of LCTR-series

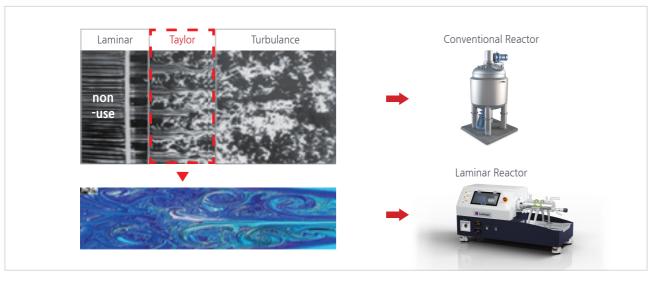
Continuous production

Possible to produce the volume same as you inject under the continuous production system



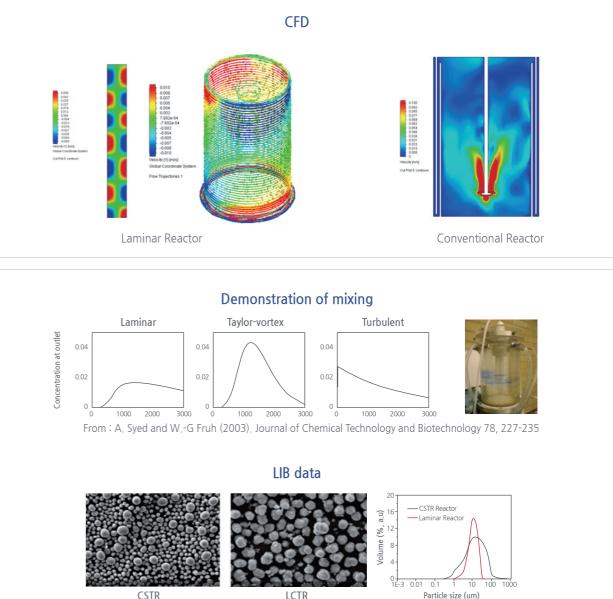
Improvement of properties

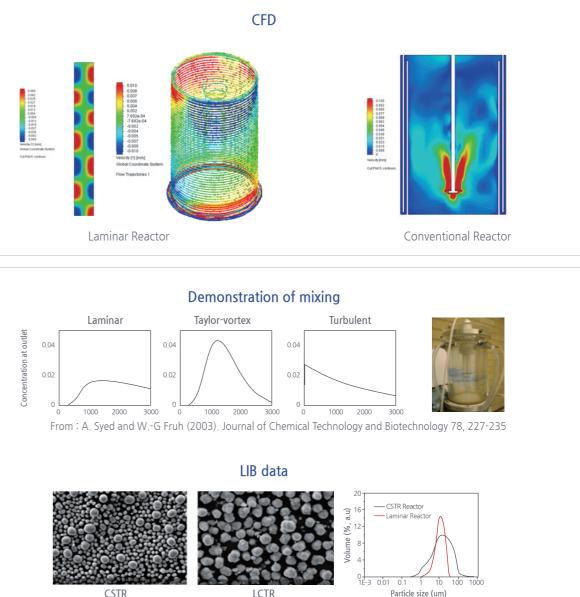
Possible to be uniformly mixed due to the vortexes regularly created

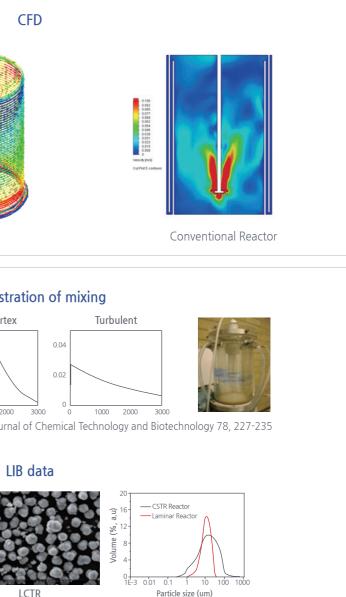


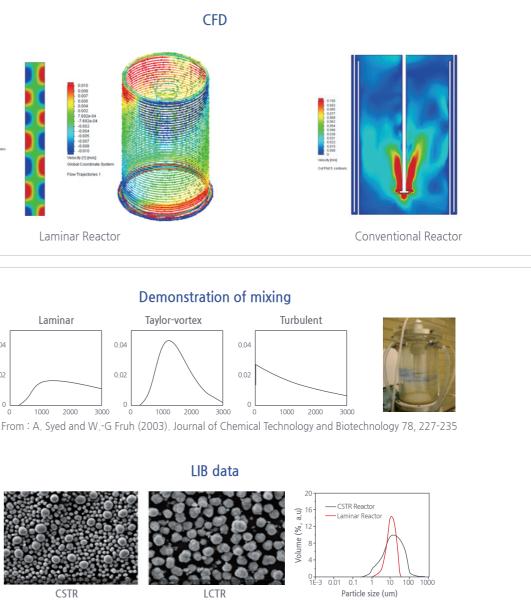
High-purity materials

Possible to reduce the formation of impurity due to that there is no any dead-zones in the reactor as an ideal fluid flow









LCTR[®]-series Laminar Continuous Taylor Reactor





 $\mathsf{LCTR}^\circ\text{-}\,\mathsf{Lab}\,1\!\!\mathrm{I}\,\text{-}\,V$

	LCTR [®] - Mini - V
Capacity (mL)	20
Max. rotation speed (rpm)	1500
Material	SUS316L & Glass & Teflon
Dimension L/W/H (mm)	274 x 525 x 617
Weight (kg)	40

	LCTR [°] - Lab II - V	LCTR° - Lab II - H
Capacity (mL)	100	200
Max. rotation speed (rpm)	1500	1500
Material	SUS316L & Glass & Teflon	SUS316L & Glass & Teflon
Dimension L/W/H (mm)	500 x 500 x 1178	1102 x 450 x 574
Weight (kg)	85	120

* Available on request



$\mathsf{LCTR}^{\circ}\text{-}\operatorname{Lab} {\rm I\hspace{-.1em}I} \text{-} H$

* Available on request

LCTR[®]-series Laminar Continuous Taylor Reactor







LCTR[®]- Tera 3100 (General Type)

LCTR [®] - Tera 3300
(PLC Type, CE Certified)

	LCTR [®] - Tera 3100	LCTR [°] - Tera 3300
Capacity (L)	1	1
Max. rotation speed (rpm)	1500	1500
Material	SUS316L & Teflon	SUS316L & Teflon
Dimension L/W/H (mm)	1470 x 700 x 1157	1400 x 700 x 1150
Weight (kg)	450	650

	LCTR [°] - Peta	
Capacity (L)	10	50
Max. rotation speed (rpm)	1500	1200
Material	SUS316L	SUS316L
Dimension L/W/H (mm)	2330 x 700 x 1220	3400 x 1300 x 1600
Weight (kg)	1200	3000

* Available on request

LCTR[®]- Peta

* Available on request

LCTR[®]-series Laminar Continuous Taylor Reactor



LCTR[®]- Exa

		LCTR [®] - Exa	
Capacity (L)	100	500	1000
Max. rotation speed (rpm)	300	250	250
Material	SUS316L	SUS316L	SUS316L
Dimension L/W/H (mm)	5800 x 2300 x 1850	6500 x 2500 x 2000	8500 x 3000 x 2300
Weight (kg)	5000	15000	25000

* Available on request

LCTR[®] Application fields

	Product			
LiFePo ₄	Ba(NO ₃) ₂	NiSO ₄		
(NiMnCo)(OH) ₂	KNO ³	CoSO ₄		
Li ₂ CO ₃	NaHCO ₃	TiO ₂		
CaCO ₃	Durene	Methionine		
K ₂ CO ₃	Diiodobenzene GMP		Diiodobenzene	GMP
NH ₄ H ₂ PO ₄	Triiodobenzene	IMP		
Nal	Lysine Graphen		Lysine	Graphene Oxide
SiO ₂	Tryptophan	SMZ		
	Manufacturing process			
Crystallization	Sol-gel process Impregnation			
Re-crystallization	Polymerization Extraction			
Co-precipitation	Radical reaction	Core-shell process		

	Product		
LiFePo ₄	Ba(NO ₃) ₂	NiSO ₄	
(NiMnCo)(OH) ₂	KNO ³	CoSO ₄	
Li ₂ CO ₃	NaHCO ₃	TiO ₂	
CaCO ₃	Durene	Methionine	
K ₂ CO ₃	Diiodobenzene	GMP	
NH ₄ H ₂ PO ₄	Triiodobenzene IMP		
Nal	Lysine	Graphene Oxide	
SiO ₂	Tryptophan	SMZ	
	Manufacturing process		
Crystallization	Sol-gel process	Sol-gel process Impregnation	
Re-crystallization	Polymerization	Extraction	
Co-precipitation	Radical reaction	Core-shell process	
Precipitation	Coating	Exfoliation	





Electronic material

Battery





Bio

Food



Petrochemistry



Environment



Medicine



Fine chemical

General types Reactors

Laminar co., Ltd is manufacturing all purpose of reactors based on our own technologies.



Tubular reactor



Catalytic reactor



Autoclave



Emulsifying device

Option



Centrifuge

Flowmeter

Solid-liquid separation Use at the tail of a reactor Use or non-use depending on the powder condition



Proposed in accordance with the process conditions



Circulator

Temp. control of the reaction solution $-25 \sim 150 \text{ °C}$



Solution feeding pump for Lab.

Max 20 mL/min Max 6 bar Materials : PP or PTFE



pH controller

Control by PID







Feeding of powder to the reactor or a storage tank 0.1 ~ 1000 g/min Materials : SS41

Solution feeding pump for production

Max 200 L/min Max 16 bar Materials : PTFE

Electronic scale (weigh the feeding quantity)

Alternative to a flowmeter 0.01 ~ 10 kg 0.001 ~ 1 kg

Solution feeding pump for slurry material

Max 600 rpm Max 8 bar





pH sensor

Acid & alkali solution For slurry